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# *Advanced Air Separations Using Novel Mixed Matrix Membranes*

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**LRS # INL/MIS-19-53293**

## Project Description and Objectives

- The objective of this project is develop an air separation technology to be utilized in **advanced fossil energy based modular energy systems** that will make substantial progress toward enabling cost-competitive, **coal-based power generation and small scale modular gasification plant** with near-zero emissions.
- The **Advanced Energy Systems (AES) program** focuses on improving the efficiency of coal-based power systems, increasing plant availability, and maintaining the highest environmental standards.
- **This project supports the Gasification Systems Program** element of AES that is developing advanced technologies to reduce the cost and increase the efficiency of modular systems.

### Strategic Alignment with Fossil Energy Objectives

*This project supports the US Clean Coal Program by focusing on developing advancements in technology that increase the performance, efficiency and availability of existing and new coal-fueled power generation to provide the United States with the best opportunity to maximize the full potential of its abundant fossil energy resources in an environmentally sound and secure manner.*

Technical Goal:  
Deliver a stream of oxygen enriched air (O<sub>2</sub> 90-95%) suitable for use in a 1-5 MWe coal fired small modular power plant

## Project Objectives and Status

- **Overall Project Goal: Develop membrane materials and processes that have the ability to generate a 90-95% O<sub>2</sub> stream from air**
  - **TECHNICAL BARRIER: Low selectivities or poor permeabilities limit membrane utility**
  - *Develop the knowledge needed to form lab scale hollow fiber (HF) membranes with predictable performance translatable to larger scale manufacturing*
  - *Membranes will be suitable for manufacturing: commercially applicable hollow fiber format*
  - *Membranes need to be durable and fouling resistant*
  - *Project scope includes materials optimization and characterization, scale up, and techno-economic assessment based on performance and predicted CAPEX, OPEX, and COE.*
  - *Overall scope addresses 3 budget periods*
- **Advantages of the INL/ANL Mixed Matrix Membrane approach**
  - *Lower energy consumption – no need to heat the gas stream or use heat/power to condense or desorb O<sub>2</sub>*
  - *Engineering to develop and deploy large surface area membrane modules is mature*
  - *Potentially lower capital cost (CAPEX)*
  - *Modular, ease of deployment*
  - *Flexible – designed to interface well with variable load demands.*

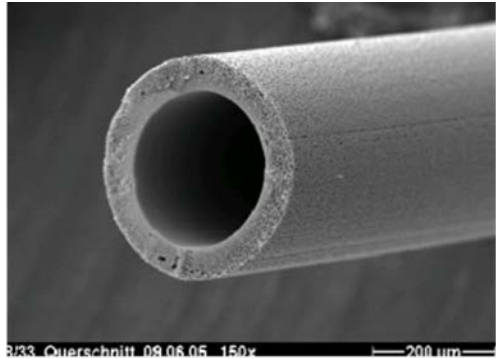
## Status at Beginning of the Project

**Driving question** – *how can membrane performance be improved to provide a **viable and less energy intensive alternative** to cryogenics, pressure swing absorption, or high temperature membrane processes for providing **90-95% O<sub>2</sub>** to support oxycombustion in small modular coal fired power plants or gasification systems?*

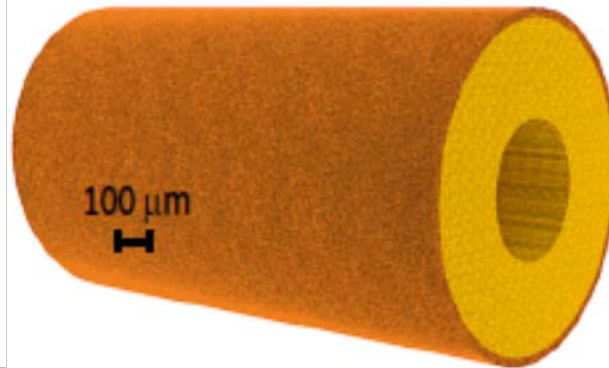
### Technical questions that must be addressed to reach the project goal:

1. Hypothesis: Nanodiamonds (NDs) in a MMM material can increase membrane permeability and selectivity. Can this be shown?
2. Do NDs impact or influence membrane formation behaviors?
3. Can we characterize the materials to yield structure-function relationships and can these be translated to the HF format?
4. How do polymer/membrane formation and behaviors influence cost of oxygen?

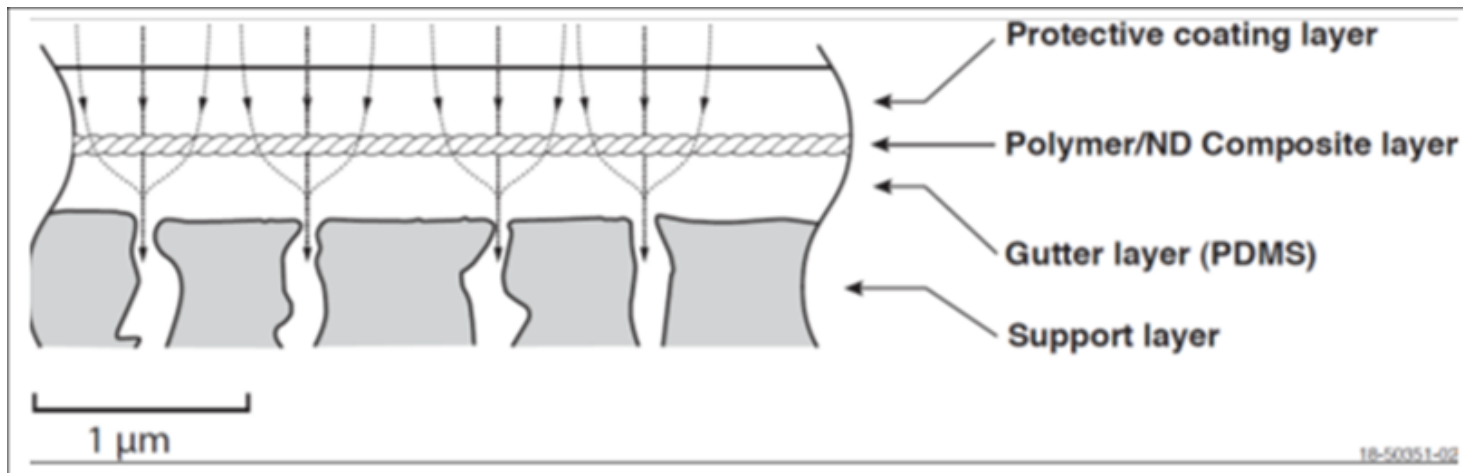
# Functional Hollow Fibers (HF) are the End Goal (HF Anatomy)



**Hollow Fiber Cross-Section**



**Hollow fiber support material**

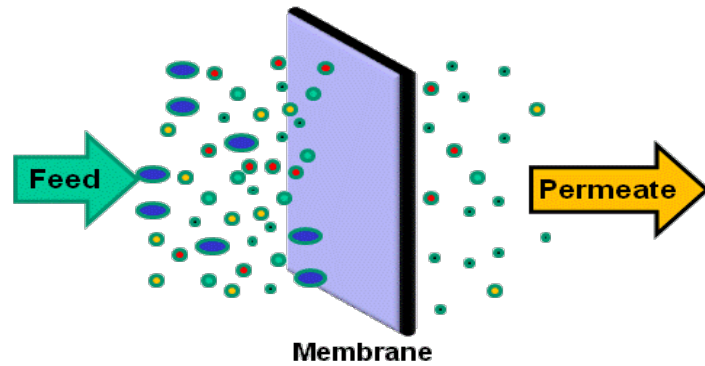


Multi-layer asymmetric membrane cross-section.

## BP1 Technical tasks:

- 1) Develop optimized PSF supports through ND screening/inclusion and membrane characterization
- 2) Optimize/improve gutter layer performance

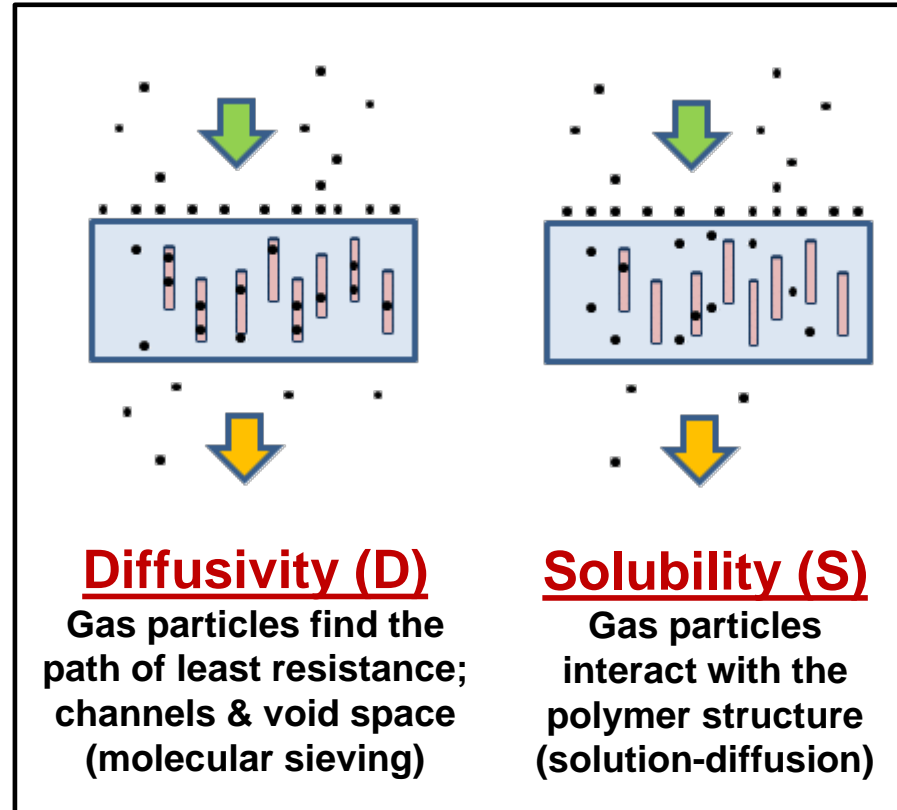
# Gas Transport Mechanisms



$$P = D \cdot S$$

Permeability      Diffusivity      Solubility

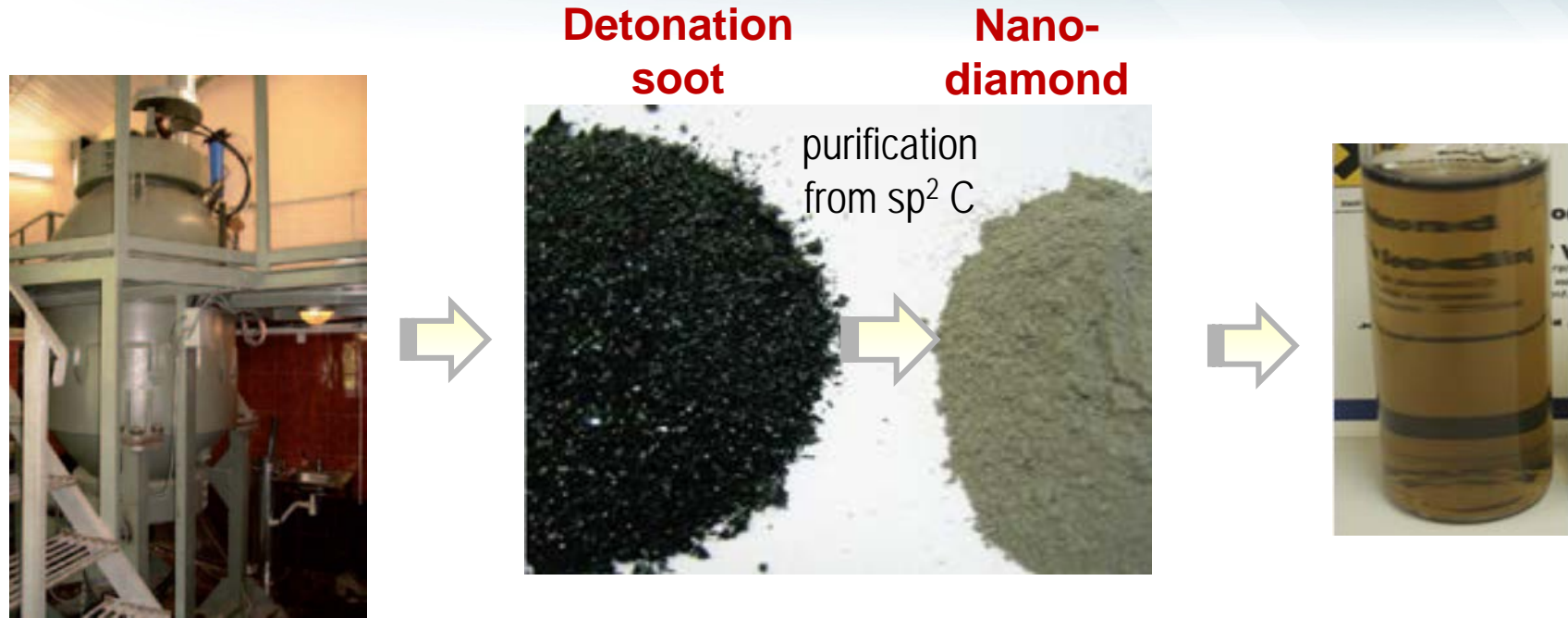
- **Permeability (P)** - product of overall gas transport.
- **Diffusivity (D)** - pressure-induced transport of gases through the polymer matrix (molecular sieving).
- **Solubility (S)** - interactions between the gases and polymer matrix (sorption).



*Both mechanisms can be manipulated in our approach to achieve the goals of this project*

$$\text{Selectivity} = P_A / P_B$$

# Nanodiamond Purification



*Control of the dispersal critical to being able to load these symmetrically into the polymer host*

## Purification from sp<sup>2</sup> carbon:

- up to 40% of cost of DND
- 35L of acids are needed for 1 kg of DND
- purification using Ozone\air mixture  
(*U.S.Patent 8,389,584; Shenderova et al. J.Phys Chem C, 2011*)

**Annual world production of detonation soot: ~4-5 tons**

**Cost of detonation soot: \$500-\$900/kg**

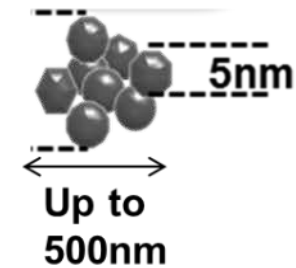
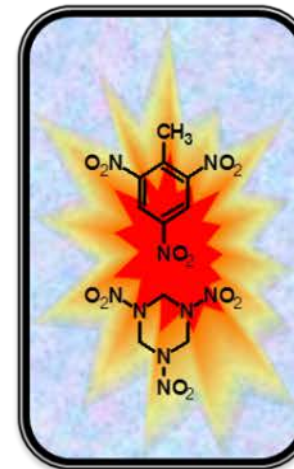
**Cost of ND: \$1500-\$40,000/kg**

# Nanodiamond Formation and Properties

- Can be as small as 3-5nm (large surface area 250-450 m<sup>2</sup>/g)
- Chemically inert and mechanically stable crystalline diamond core
- Non-toxic & biocompatible
- Reactive surface: can be customized for specific applications
- Possess functional defects in the lattice
- Produced in large quantities (tons/ year)

## ND of Dynamic Synthesis

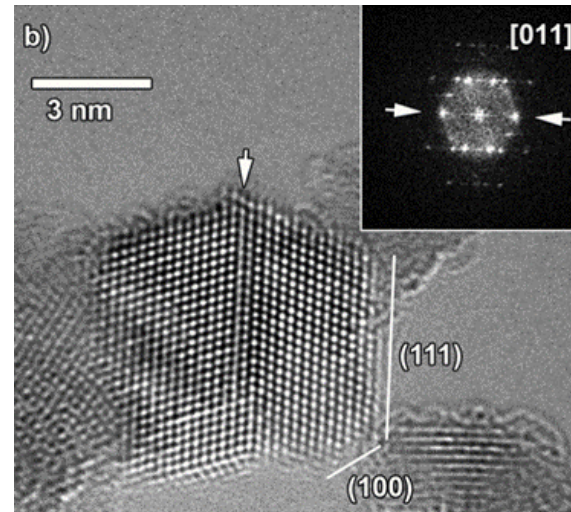
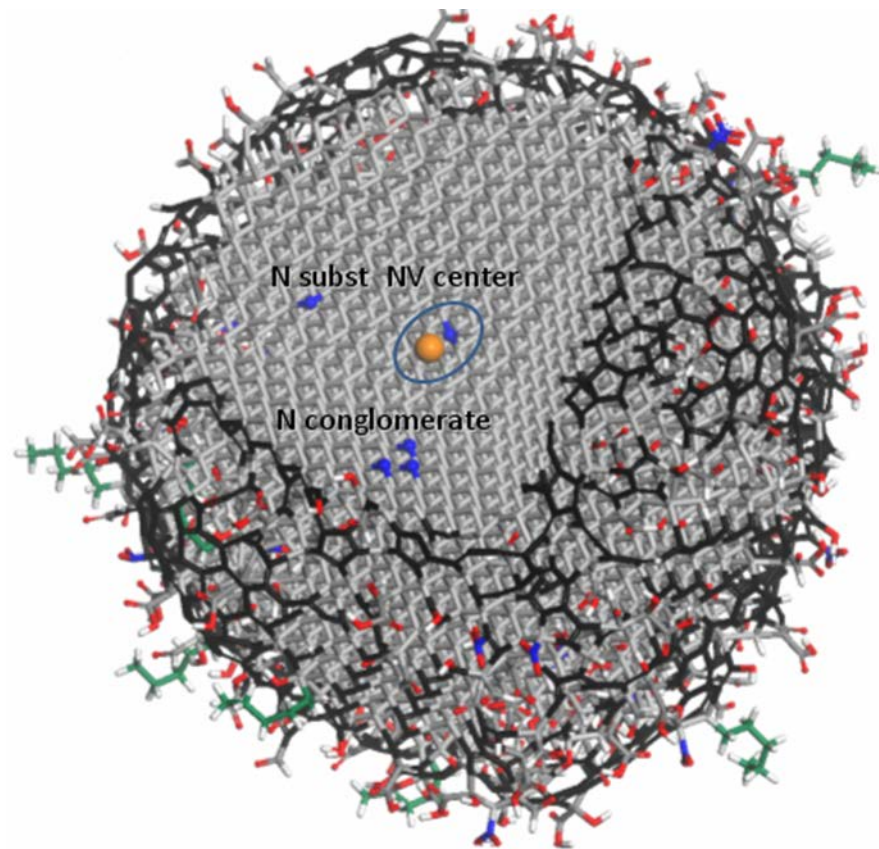
Detonation Nanodiamond (DND)



NDs can be:  
 1) completely deagglomerated into individual particles, or 2) clustered into porous structures



# ND functionalization – Influencing Diffusivity and Solubility



**Surface functionalization to influence particle zeta potential, hydrophobic/hydrophilic balance**

Also expected to influence dispersal in solvent

Agglomeration influences **gas diffusion** through induced porosity

Surface chemistry may influence **gas solubility**

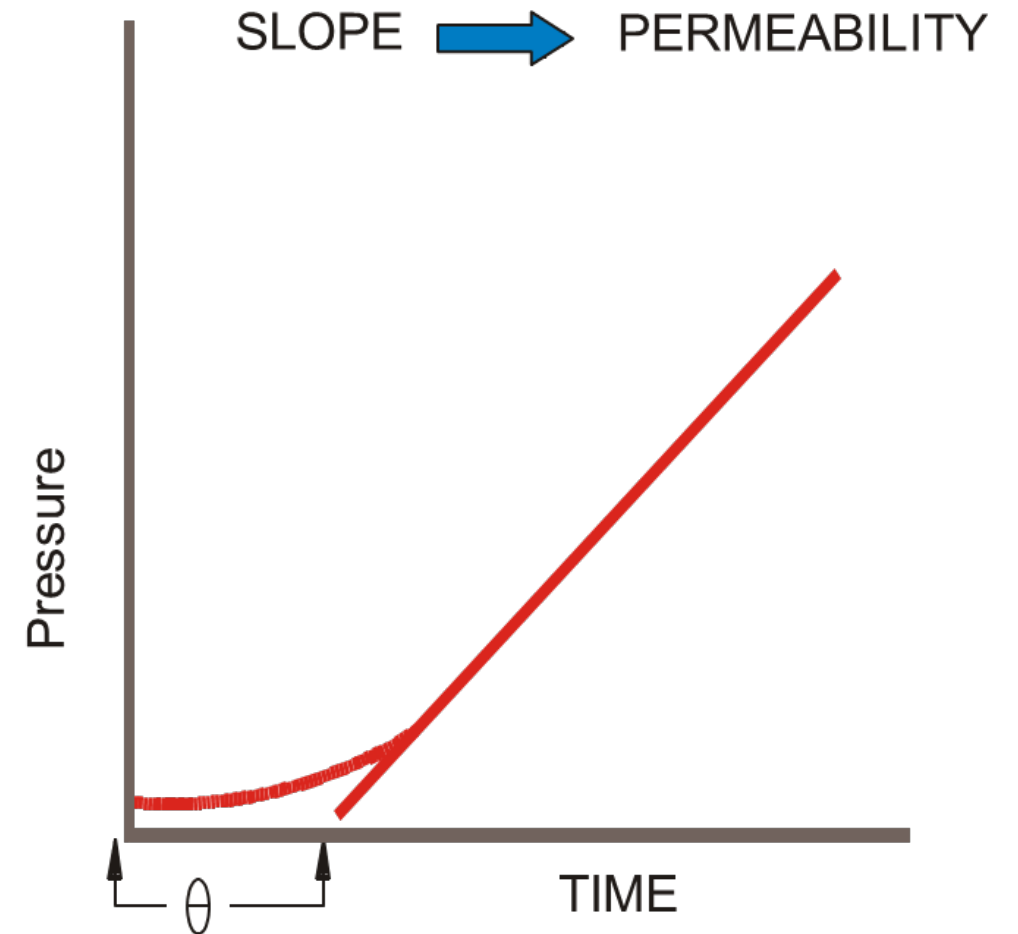
V.Mochalin, O.Shenderova, D.Ho, Y.Gogotsi, *Nature Nanotech*, 2012  
 Book *Ultrananocrystalline Diamond* (Eds Shenderova, Gruen), 2012

# Experimental Methods – Pure gas measurements



## Barometric Technique

- Feed pressure: 30 psi
- Low temperature: <100 C



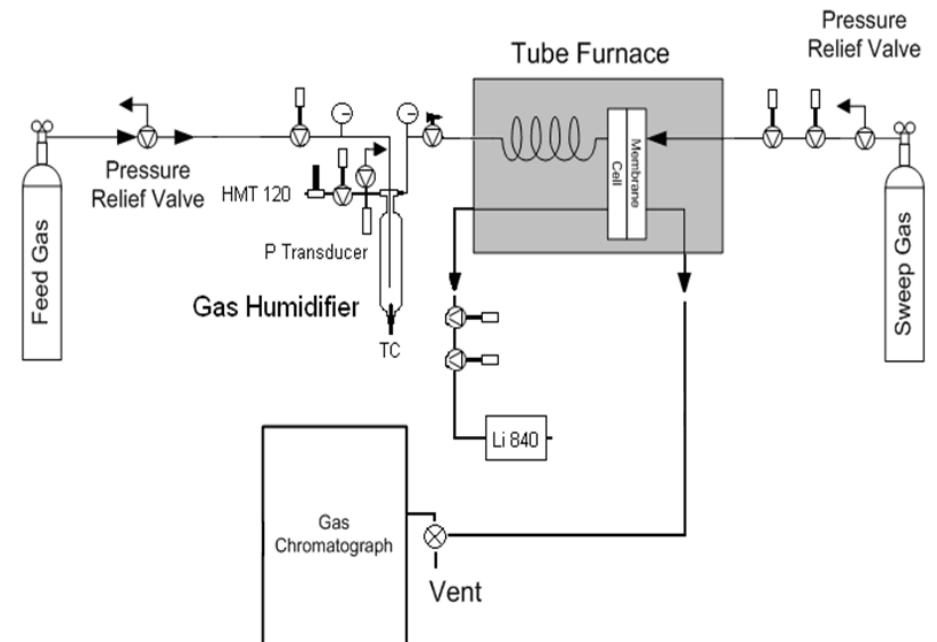
# Mixed Gas Analysis



## Analytical Technique

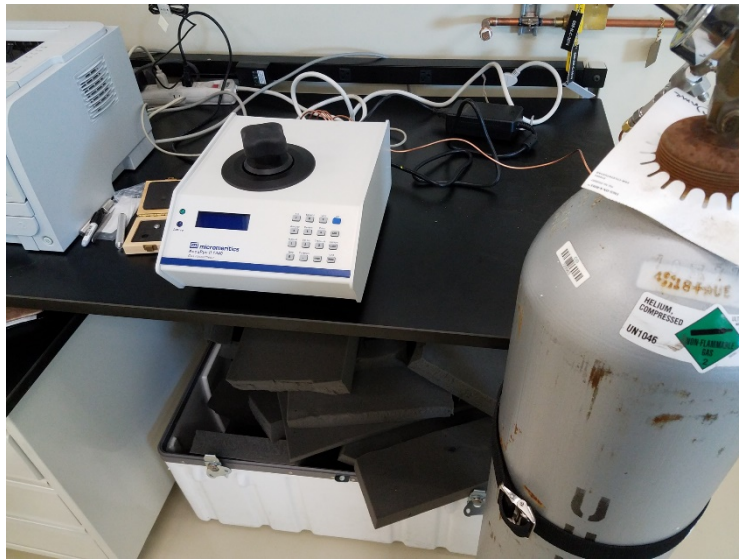
Two systems that differ by  
Temperature control

- Low temperature: <100 C
- Higher Temperature: <500 C



## Current Status of the Project

- **Results compared to benchmark** – New start, establishing benchmarks for permeability, selectivity
  - Early results match well with benchmark literature values
  - Collection of other data such as **density**, **thermomechanical behavior** (initiated), and **positron annihilation lifetime spectroscopy (PALS)**.
- **Describe how/if objectives have changed** – Nothing has changed



Helium pycnometry for “hyper-accurate” densities



Thermal analysis suite for measuring physical properties

## ***Project Update/Accomplishments***

- **Administrative tasks to support project initiation**
  - Technical and administrative tasks begun early January, 2019.
  - Project kickoff meeting completed January 22, 2019
  - MPO to Argonne National Laboratory completed in February (\$250K)
  - Travel to Adamas Nanotechnologies (Raleigh, NC) February 11, 2019
    - Selection and acquisition of nanodiamonds
  - Acquired polysulfone (PSF) polymer, membranes, and other materials necessary to begin work
- **First steps moving forward:**
  - Performance Benchmarking
    1. Techniques for performance measurements
    2. Pure polysulfone (PSF) and polydimethylsiloxane (PDMS)
    3. Identify nanodiamonds – porosity, agglomeration, surface functionalization
  - Membrane Formation – **NDs appear to aid in defect free membrane formation**
- **Technical and/or collaborative challenges** – choosing the correct materials for the permeability testing – examples: PDMS vs Viton or-ring seals and sealing cells.

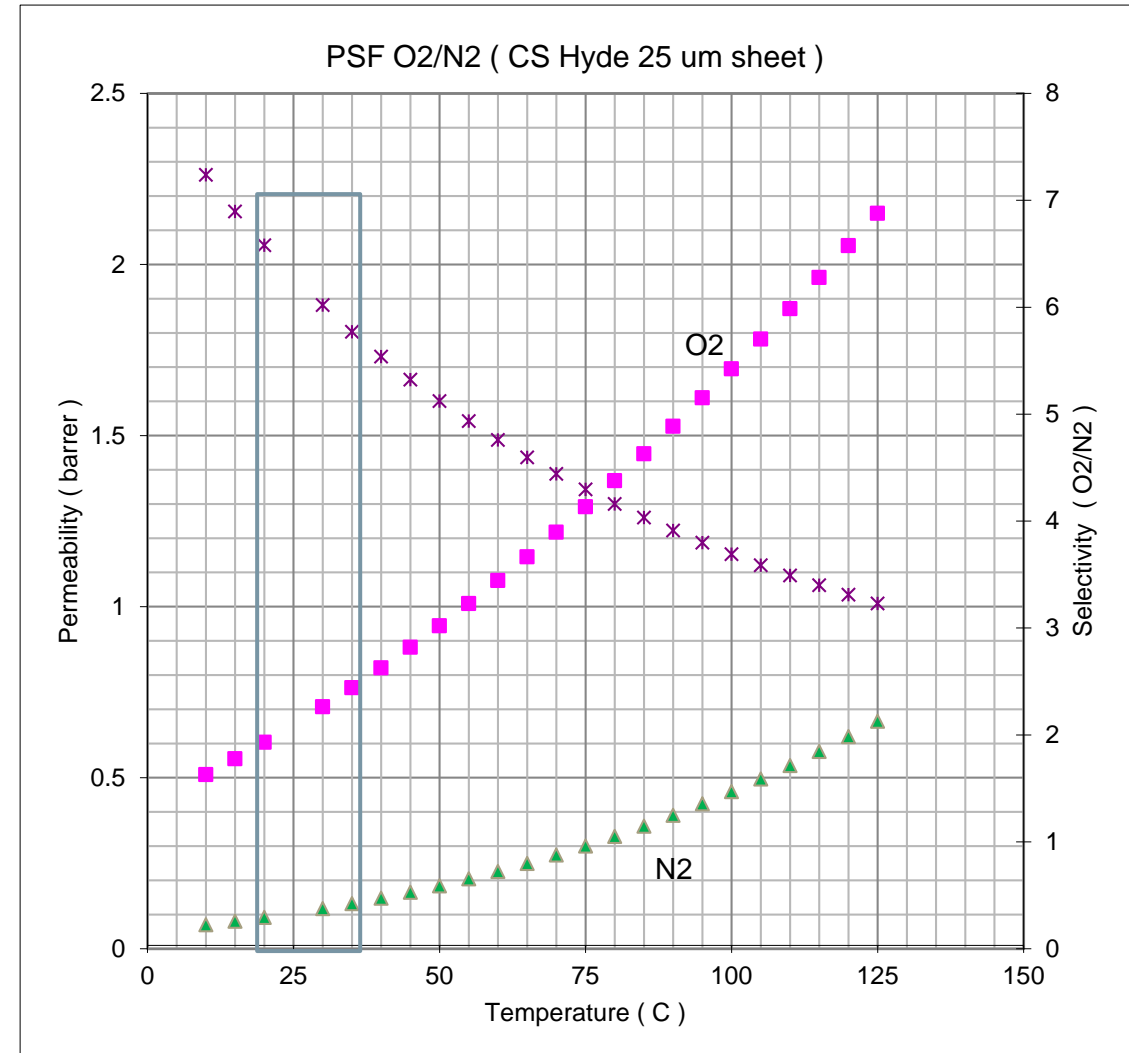
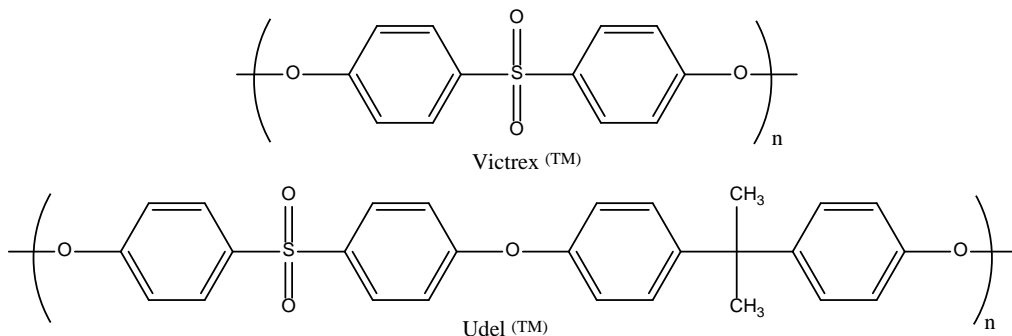
## Industry/input or validation - Benchmarking PSF

Membrane Material	O <sub>2</sub> Permeability (Barrer)	O <sub>2</sub> /N <sub>2</sub> Selectivity	Additive	Reference
PSF/CNF mixed matrix	2.2	3.86	Carbon Nanofiber	1
PSF with 20% silica nanoparticles	5.0	4.50	Silica	2
PSF with 5% $\mu$ CX	15.3	7.03	Zeolite	3
PSF with 5% CX	17.8	5.95	Pyrolytic Carbon	4
Pure PSF	1.2	6	None	5

1. Kiadehi, A.D.; Rahimpour, A.; Jahanshahi, M.; and Ghoreyshi, A.A. (2015). "Novel carbon nano-fibers (CNF)/polysulfone (PSf) mixed matrix membranes for gas separation", *Journal of Industrial and Engineering Chemistry*, 22, 199-207.
2. Golzar, K.; Amjad-Iranagh, S.; Amani, M.; and Modarress, H. (2014). "Molecular simulation study of penetrant gas transport properties into the pure and nanosized silica particles filled polysulfone membranes", *Journal of Membrane Science*, 451, 117-134.
3. Weng, T.-H.; Wey, M.-Y.; and Tseng, H.-H. (2010). "Enhanced O<sub>2</sub>/N<sub>2</sub> separation performance of poly(phenylene oxide)/SBA-15/carbon molecular sieve multilayer mixed matrix membrane using SBA-15 zeolite particles", *Proceedings from the 2010 International Conference on Chemistry and Chemical Engineering*, Kyoto, Japan, 245-248.
4. Magueijo, V.M.; Anderson, L.G.; Fletcher, A.J.; and Shilton, S.J. (2013). "Polysulfone mixed matrix gas separation hollow fibre membranes filled with polymer and carbon xerogels", *Chemical Engineering Science*, 92, 13-20.
5. Robeson, L.M. (1999). "Polymer Membranes for Gas Separation", *Current Opinions in Solid State and Materials Science*, 4, 549.

# Project Results: Technology Benchmarking – Pure PSF

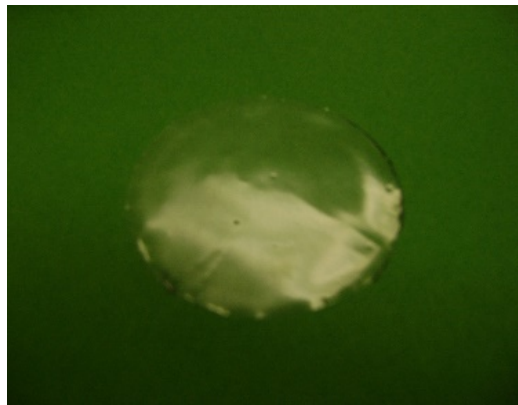
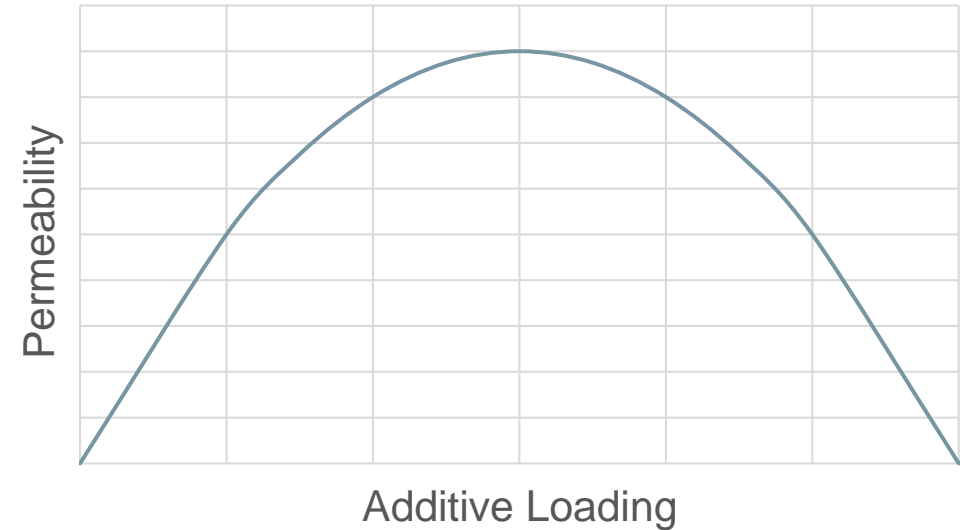
- Analysis based on pure gas determinations of O<sub>2</sub> and N<sub>2</sub> permeability taken at 3 temperatures (20, 30, and 40 °C)
  - Data calculated from an Arrhenius relationship
  - Ideal selectivity =  $\alpha = P_{O_2}/P_{N_2}$
- PSF chosen for several reasons:
  - Predictable performance
  - Commercially available
  - Readily formed into flat sheet membranes and hollow fibers



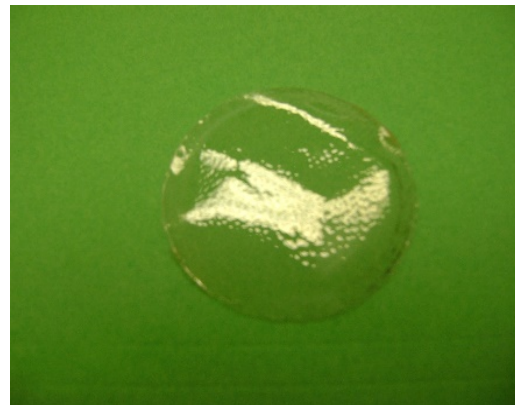
# Understanding MMM formation

Loading of materials into polymers

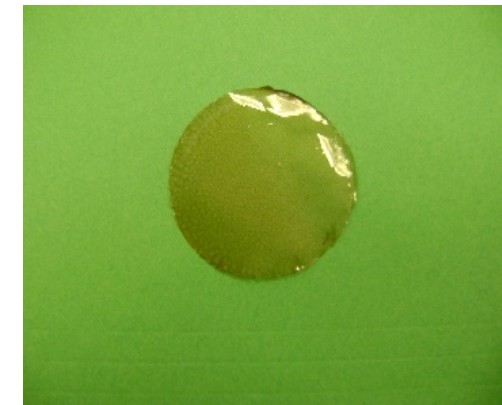
- Experiments begun with:
  1. Zeolites: to probe the effect of porous additives (3, 4, and 5 Å pores)
    - Expected: 3Å enhances  $\alpha$  but water sensitive
    - 5 Å exhibits little selectivity
  2. Functionalized NDs
    - Initial result: The expected relationship between P and loading %



25 µm Udel PSF membrane



Udel PSF with 5% ND



Udel PSF with 10% ND Aggregate



## ***Summary: Progress on Technical Questions***

- Do NDs in a MMM material increase or decrease permeability and selectivity?
  - Status: We do not know. We have just started to collect gas permeability data – need more replicates before data can be published.
- Do NDs impact or influence membrane formation behaviors?
  - YES. NDs tend to add viscosity to membrane casting solutions that assists in forming defect free films. This is an important observation and will enable HF formation
- Can we characterize the materials to yield structure-function relationships and can these be translated to the HF format?
  - YES. ANL will be conducting permeability tests to support INL's work. Also, at INL we have a post-doc who will perform SEM and are hiring an intern for thermal analysis.
  - Film forming improvement may be due to chemistry between the polymer and ND – should be reflected in the glass transition temperature ( $T_g$ ) – experiments on-going
- How do polymer/membrane formation and behaviors influence cost of oxygen?
  - Status: We do not know at this time; however we have a new INL staff member (former post-doc) who has begun to develop an ASPEN Plus flowsheet to allow us to computationally compare approaches

## ***Preparing Project for Next Steps: Technical***

- **Continue to investigate Permeability and Selectivity as a function of:**
  - Focus on flat sheet geometry – quick and easy to screen a variety of formulations
  - ND loading
  - Choice of ND (functionalization)
  - Temperature
  - Polymer – both substrate and gutter layers (PSF and PDMS)
- **Characterize membranes**
  - DMA – Mechanical behaviors as a function of temperature
  - TGA - Thermal stability
  - DSC – Glass transitions, molecular interactions between polymer host and NDs
  - Microscopy – Defect structure
  - Porosimetry
  - Density – quick and easy proxy for fractional free volume
  - Positron Annihilation Lifetime Spectroscopy – Fractional free volume and its link to gas permeation.
- **Set up for successful HF formation – ensure that critical attributes will translate from film to fiber**

## *Preparing Project for Next Steps*

- **Market Benefits/Assessment**

- Market is mature for membrane systems giving 99.5% N<sub>2</sub> or 30-50% O<sub>2</sub>
- Membrane systems yielding 90-95% O<sub>2</sub> not mature
- Growing market - \$1.3 billion by 2025, Predicted Compound Annual Growth Rate (CAGR) of 8.4% (2015-2025).\*
- **Complete Techno- Economic Assessment of this work planned for BP3**
- Applications for low-cost oxygen enrichment: medical (45%), enhanced combustion (20%), water treatment (25%)

- **Technology to Market Path**

- Protection of Intellectual Property (**INL Invention Disclosure Record expected by 7/1/2019**)
- Engage INL Technology Deployment and Industrial Engagement staff to support agreements management and licensing, market research, etc.
- Bridging from this project to industry
  - ARPA-E
  - SBIR
  - SPP, CRADA, others

\* Creedence Research, 2018 ([www.credenceresearch.com/press/global-oxygen-enriched-membrane-market](http://www.credenceresearch.com/press/global-oxygen-enriched-membrane-market))

## Concluding Remarks

- **Overall Project Objectives:** Enable small modular coal fired gasification while minimizing environmental impact
- **Applicability of the Technology to FE objectives:** *Air separation technology to be utilized in **advanced fossil energy based modular energy systems** that will make substantial progress toward enabling cost-competitive, **coal-based power generation with near-zero emissions***
- **Project Status – new start 12/1/2018.**
- **Budget Period 1 Technical Milestones: On-schedule**
  - Complete initial flat sheet membrane formation study to demonstrate defect-free films can be made, optimize the ND loading (10/30/2019)
  - Complete study of flat sheet membrane suitable for publication (11/30/2019)

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